

CLAIM AMENDMENTS

Amended claims: 1,2, 4-6. Cancel claim 3.

1. (Currently Amended) A process Process for the preparation of a gas containing hydrogen and carbon monoxide containing gas from a carbonaceous feedstock, the process comprising by performing the following steps:
 - (a) partial oxidation of partially oxidizing a carbonaceous feedstock in an a vertically oriented tubular partial oxidation reactor vessel having an upper end, and a lower end having an inlet, the vessel comprising a burner at its the upper end thereby obtaining a first gaseous product of hydrogen and carbon monoxide having a temperature between 1100 °C and 1500 °C[[],]];
 - (b) catalytic catalytically steam reforming a carbonaceous feedstock in the presence of steam in a Convective Steam Reformer Zone convective steam reformer zone thereby obtaining a steam reformer product[[],]];
 - (c) reducing the temperature of the first gaseous product of step (a) by between 300 °C and 750 °C by mixing this the first gaseous product with the steam reformer product of step (b) by feeding the steam reformer product into the said inlet yielding a first mixture;
 - (d) contacting the first mixture obtained in step (c) with a bed of reforming catalyst positioned in the lower end of the partial oxidation reactor vessel just below the position said inlet and obtaining a second mixture having a temperature between 950 °C and 1100 °C at which the steam reformer product is fed to said reactor,; and
 - (e) providing the required heat for the convective steam reforming reaction zone in step (b) by convective heat exchange between the second mixture obtained in step (d) having a temperature between 950 °C and 1100 °C and the steam reformer reactor zone thereby obtaining a hydrogen and carbon monoxide containing gas having a reduced temperature.
2. (Currently Amended) The process of Process according to claim 1, wherein the steam to carbon molar ratio of the feed to step (b) is between 0.5 and 0.9.

3. Cancel.

4. (Currently Amended) The process ~~Process according to any of claims 1[[-3]]~~, wherein the content of methane in the steam reformer product is between 1 mol% and 10 mol% relative to the carbon present as hydrocarbon in the carbonaceous feed to step (b).

5. (Currently Amended) The process ~~Process according to~~ of claims 1[[-4]], wherein the methane conversion in step (d) is between 10 wt% and 50 wt%.

6. (Currently Amended) The process ~~Process according to~~~~Process according to any one of claims 1[[-5]]~~, wherein the temperature of the mixture obtained in step (d) is between 980 °C and 1050 °C.